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(54) Ethyl guar, a method for its preparation and use thereof

(57) A process is provided for making alkylated galactomannans comprising reacting a galactomannan in the presence of sodium hydroxide, water, and an alkyl halide to form a reaction mass under pressure and at temperatures greater than 50°C in amounts and for a time sufficient to achieve a degree of substitution greater than 2.4. Organic volatiles from the reaction mass are stripped and the reaction mass is then washed in water at temperatures high enough to prevent dissolution or agglomeration of the alkylated galactomannan. This washed product is then dried and pulverized to suitable particle size. This product is useful in applications requiring thickening and rheology modification of formulations containing organic solvents or formation of coatings/film from organic solvents. The products are also useful in pharmaceutical applications.

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alkali is necessary to promote the reaction with the alkylating reagent, the highest molecular weights are retained by rigorous removal of as much oxygen as possible from the system. Lower molecular weight can be achieved, if desired, by less rigorous exclusion of oxygen or purposeful injection of air into the reaction mass.

An alternative method for producing lower molecular weight products is to add a chemical oxidant, such as an inorganic peroxide like hydrogen peroxide or an organic peroxide like t-butyl hydroperoxide, to the reaction mass. The use of chemical oxidants, particularly in combination with metal ion catalysts such as iron and cobalt, to reduce molecular weight of polysaccharides is also well known in the art.

In the present invention, the base is preferably an alkali metal hydroxide such as sodium hydroxide. The concentration of the base and the concentration of water added to the galactomannan are variables affecting the ultimate degree of substitution of the product and the reacting efficiency of the alkylating reagent. The concentrations can vary widely depending on the desired degree of substitution and the nature and concentration of the alkylating agent. The presence of an inert diluent may also be a factor in determining the concentration of the base. The use of an excess amount of sodium hydroxide above the stoichiometric amount required to achieve the desired degree of substitution is preferred in this invention.

In this invention, an inert diluent is not necessary, but may be added to aid stirrability of the reaction mass and promote better heat transfer. Preferred diluents are immiscible with water and are unreactive to the base or alkylating reagent. Most preferred diluents are aliphatic or aromatic hydrocarbon solvents such as heptane, toluene, or xylene.

As the next step in the process of the present invention, an alkylating reagent is added to the alkalinized galactomannan slurry and reacted at elevated temperature. The preferred alkylating reagent is an alkyl halide or mixtures thereof, wherein the alkyl group is methyl, ethyl, or propyl and the halide is chloride, bromide, or iodide. For practical considerations, methyl chloride and ethyl chloride are preferred, with ethyl chloride being most preferred. The concentration of the alkyl halide can vary widely depending on the desired degree of substitution, alkylating reagent, presence of a diluent, reaction time and temperature, and concentrations of sodium hydroxide and water in the reaction mixture. All these factors can affect the reaction efficiency of the alkyl halide with the galactomannan. It is the reaction efficiency of the alkylating reagent under the reaction conditions and desired degree of substitution that determines the concentration of the alkylating reagent. A preferred mode of operation uses an excess of alkylating reagent above and beyond that required to achieve the desired degree of substitution. Unreacted alkylating reagent at the end of the reaction may be recovered and recycled.

With these considerations in mind and the realization that reagent concentrations can vary widely within

the spirit of this invention, a preferred process for manufacturing organo-soluble ethylated galactomannan with an ethyl DS greater or equal to about 2.4 uses about 5.0 to 8.0 parts sodium hydroxide to 1 part galactomannan, about 4.0 to 6.5 parts water to 1 part galactomannan, and about 3.0-5.0 parts ethyl chloride to 1 part galactomannan.

In the most preferred process, the sodium hydroxide is predissolved in the water before being added to the galactomannan. About 11.5 parts of sodium hydroxide solution to 1 part galactomannan is used, and the ethyl chloride is in the range of about 3.5 to 4.5 parts. The ethyl DS is varied by adjusting the strength of the sodium hydroxide-water solution from about 45 to 65 wt% sodium hydroxide or by varying the amount of ethyl chloride charged to the reactor.

After adding the sodium hydroxide, water, and ethyl chloride to the pressure reactor, and optionally any molecular weight degrading reagent, the pressure reactor is sealed and heated. The reaction time and temperature can vary widely depending on the specific alkylating reagent used. In a preferred process using ethyl chloride to make ethylated galactomannan, the reactor is heated slowly to 90-100°C over 4 hours, held at that temperature for 1-3 hours, then heated slowly to 140°C over about 3 hours, and held at that temperature for 1-2 hours.

Alternatively, the reactor may be heated slowly to about 140°C over about 5 hours and held at that temperature for about 3 hours. The pressure at the end of the reaction may reach as high as 500 psi. The reactor is then slowly vented while at 130-140°C to remove volatile organic components.

After venting, the reactor is cooled and discharged. The crude product is then washed with water to remove water-soluble components. The temperature of the water during washing will vary depending on the DS of the product. For ethylated galactomannans with DS values greater than about 2.7, the temperature of the water can be as low as about 25°C. For products with DS values less than about 2.6, it is preferred that the water temperature be greater than about 40°C to inhibit excessive swelling of the product. During washing, an acid such as acetic or hydrochloric acid, may be added to neutralize residual sodium hydroxide. Also, an oxidizing agent such as an organic or inorganic peroxide may be added to degrade the molecular weight of the alkylated galactomannan. Washing with water, either in batch or continuous mode, is continued until the desired level of purity is achieved. Thereafter, the product is dried and ground to the desired particle sizes.

In accordance with this invention, the alkylated galactomannans produced from this process have an alkyl degree of substitution (DS) greater than 2.4 and are soluble in, and effectively thicken, many organic solvents. Typical organic solvents which ethyl guar is soluble in, include alcohols such as methanol and ethanol and furfurals, ketones such as methyl ethyl ketone and acetone, aromatic hydrocarbons such as toluene,

cycloaliphatic hydrocarbons such as limonene and pinene, esters such as ethyl acetate, isopropyl palmitate and alkyl benzoates, and polar aprotic solvents such as acetonitrile and dimethylformamide. Ethyl guar is poorly soluble in aliphatic hydrocarbon solvents such as heptane, but is soluble in mixtures of aliphatic and aromatic hydrocarbon solvents.

Materials with DS values greater than about 2.6 are insoluble in water at about 25°C, but become partially or mostly soluble at temperatures less than about 20°C. Materials with DS values less than about 2.6 are partially or mostly soluble in water at about 25°C, but phase out of solution and are insoluble at temperatures between about 25°C and 35°C.

The ethyl guars of this invention also tend to be thermoplastic and can be thermally-compressed into coherent films at about 175°C.

#### Example 1

##### Preparation of Ethylated Guar DS = 2.9

A 10-gallon autoclave with an agitator therein was preheated to 75°C. A nitrogen sparge was introduced. The reactor was charged with 43.5 lb of sodium hydroxide pellets or flake and 25.5 lb of water (53% solution). After dissolution of the sodium hydroxide, the vessel was cooled to 75°C and 6 lb of guar flour was added to the autoclave with the agitator turned on. The nitrogen sparge was removed, and the reactor was sealed. The reactor was further purged with nitrogen to remove the oxygen above the liquid phase in the reactor and then 26.4 lb of ethyl chloride was added. The reactor was heated at a constant rate to 140°C over 5 hours, and then held at 140°C for 3 hours. The reactor was then vented at a constant rate over 1 hour while maintaining the temperature at 130-140°C. The reacted mass was then cooled to about 50°C, dumped from the reactor, and batch washed with water. Acetic acid was used in the final washes to adjust the pH of the water slurry to 6-8. The purified product was dried and ground. It had a degree of substitution of 2.9.

#### Example 2

##### Preparation of Ethylated Guar DS = 2.8

The same procedure was followed as in Example 1 except that 40 lb of sodium hydroxide and 29 lb of water (58% solution) were used in the reaction.

#### Example 3

##### Preparation of Ethylated Guar DS = 2.7

The same procedure was followed as used in Example 1 except that 35.9 lb of sodium hydroxide and 33.1 lb of water (52% solution) were used in the reaction.

#### Example 4

##### Preparation of Ethylated Guar DS = 2.6

The same procedure was followed as used in Example 1 except that 32.4 lb of sodium hydroxide and 36.1 lb of water (47% solution) were used in the reaction.

#### Example 5

##### Preparation of Ethylated Guar Using A Different Heating Schedule

The same procedure was followed as used in Example 1 except that the reaction was heated to 100°C over 2 hours, held at 100°C for 2 hours, then heated to 140°C over 3 hours and held at 140°C for 1 1/2 hours. The products produced by this schedule typically had a DS between 2.8 and 2.9.

#### Example 6

##### Preparation Ethylated Locust Bean Gum

The same procedure was followed as used in Example 1 except that locust bean gum flour was used instead of guar. The final product had a DS of 2.7.

#### Claims

1. A process for making alkylated galactomannans comprising a) reacting a galactomannan in the presence of sodium hydroxide, water, and at least one alkyl halide to form a reaction mass heated at temperatures greater than 50°C in amounts and for a time sufficient to achieve a degree of alkyl substitution of greater than 2.4, b) stripping organic volatiles from the reaction mass, c) washing the reaction mass with water at temperatures high enough to prevent dissolution or agglomeration of the alkylated galactomannan, and d) drying and pulverizing the dried alkylated galactomannan to suitable particle size.
2. The process of claim 1, wherein the reaction takes place in the presence of a diluent.
3. The process of claim 2, wherein the diluent is selected from an aliphatic or aromatic hydrocarbon.
4. The process of claim 3, wherein the diluent is toluene or xylene.
5. The process of claim 1, wherein the reaction mass is neutralized with an acid after the stripping step during washing with water.
6. The process of claim 5, wherein the acid is either an organic acid or a mineral acid.

7. The process of claim 1, wherein the alkyl portion of the alkyl halide independently is selected from the group consisting of methyl, ethyl, propyl, or mixtures thereof.  
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8. The process of claim 1, wherein the alkyl portion of the alkyl halide is ethyl.
9. The process of claim 7, wherein the halide portion of the alkyl halide is selected from the group consisting of chloride, bromide, and iodide.  
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10. The process of claim 1, wherein the galactomannan is selected from the group consisting of guar gum and locust bean gum.  
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11. The process of claim 1, wherein the temperature of the water during the washing step is greater than 40°C.  
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12. The process of claim 1, wherein an oxidizing agent is added either to the reaction step or to the washing step in order to oxidatively degrade the alkylated galactomannan and reduce its molecular weight.  
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13. The process of claim 12, wherein the oxidizing agent is selected from the group consisting of i) oxygen in the presence of caustic, ii) inorganic peroxides, and iii) organic peroxides.  
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14. The process of claim 13, wherein the oxidizing agent is hydrogen peroxide.
15. The process of claim 14, wherein the oxidizing agent is added during the washing step.  
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16. The process of claim 12, wherein the oxidizing agent is air and is added during the reaction step.
17. The process of claim 1, wherein the reaction is conducted under an inert atmosphere.  
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18. The process of claim 1, wherein the inert atmosphere is created with nitrogen.  
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19. The product obtainable according to the process of any one of claims 1-18.
20. The use of the product according to claims 19 for the manufacture of a pharmaceutical preparation.  
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## EUROPEAN SEARCH REPORT

Application Number  
EP 95 11 6304

DOCUMENTS CONSIDERED TO BE RELEVANT			CLASSIFICATION OF THE APPLICATION (Int.CI)
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	
Y	DE-A-36 02 151 (HENKEL) * page 3, line 10 - line 44; example 5 *	1-10, 17-19	C08B37/14
Y	EP-A-0 277 499 (HENKEL) * page 1, column 1, line 33 - column 2, line 41 *	1-10, 17-19	
Y	US-A-4 547 570 (GARNER) * column 4, line 20 - line 41; example 1 *	1-10, 17-19	
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The present search report has been drawn up for all claims			
Place of search		Date of compilation of the search	Examiner
THE HAGUE		22 January 1996	Lensen, H
CATEGORY OF CITED DOCUMENTS			
X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background C : non-written disclosure P : intermediate document			
T : theory or principle underlying the invention E : earlier patent document, but published eq. or after the filing date O : document cited in the application L : document cited for other reasons A : member of the same patent family, corresponding document			